

Overview on Thermal Waste Treatment Technology

Fundamentals of Waste Incineration, Pyrolysis and Gasification
(Adapted presentation)

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Content

- Introduction
- Legal Framework (EU)
- Waste Incineration Technology
 - Grate
 - Fluidised Bed (BFB, CFB)
 - Rotary Kiln
- Flue Gas Cleaning
- Waste Water Treatment
- Energy Recovery
- Pyrolysis, Gasification

Environmental Engineering and Consulting Company

Staff: 13 persons

Offices in Vienna and Linz, AT

• Main Fields of Expertise

- Waste Management
- Thermal Waste Treatment
- Landfill Sites
- Energy Efficiency

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Activities

- Project Development
- Pre-Feasibility & Feasibility
- Permitting Procedure
- Engineering
- Commissioning
- Operation

Current Projects (Selection)

- BLRB – Engineering, Commissioning
- Energy Efficiency / Iron and Steel Industry
- Waste Management Plan for the Republic of Uzbekistan

INTRODUCTION

Properties of Waste (1)

- **Unknown composition**
- **Heterogeneous**
- May contain contaminants and hazardous components, e.g.
 - heavy metals,
 - chlorine,
 - sulphur,
 - persistent organic pollutants...

ANYTHING might come along. →

Waste Incineration Technology must be safe and sound and equipped with best available abatement technology.

Properties of Waste (2)

| MSW Composition | | Content |
|----------------------------------|------------------|---------------------|
| Carbon | C | 20 – 25 % |
| Hydrogen | H | 2 – 4 % |
| Oxygen | O | 15 – 20 % |
| Nitrogen | N | 0,3 – 1,0 % |
| Sulphur | S | 0,2 – 0,5 % |
| Water | H ₂ O | 25 – 35 % |
| Ash / Inert Material | | 20 – 30 % |
| Lower Heating Value (LHV) | | 8 – 12 MJ/kg |

Further Chemical Elements

- P, Cl, F ...
- Na, K, Ca, Mg ... *
- Fe, Ni, Cd, Pb, Hg, Cr, As, Sb ... *
- *) Partly as elements, mostly as **Ash**:
oxides, chlorides, sulphates, silicates ...

Heating Value (LCV) Range

- 3 MJ/kg (dewatered sewage sludge)
up to
- > 30 MJ/kg (plastic waste)
- **8-12 MJ/kg – typical LCV range of MSW**

Advantages of Waste Incineration

- Volume Reduction ~ 90%
 - Mass Reduction ~ 60%
 - Destruction of Organic Components →
 - → Inertisation
 - → Sanitation / Disinfection
 - Prevention of PCDD/F (Polychlorinated Dibenzo Dioxins and Furans) Synthesis
 - High Energy Efficiency for Heat and Power Production
 - Less specific greenhouse gas emissions than landfill: Global warming potential of CH₄ is 28 times higher than of CO₂
 - **Waste Incineration is the „State of the Art“ in Thermal Waste Treatment, numerous Reference Plants**
- If carefully designed and operated:**
- **Minimum Environmental Impact**
 - **Reliable & quite easy to operate**

LEGAL FRAMEWORK (EU)

Industrial Emissions Directive (IED) 2010/75/EU

- **Chapter IV and Annex VI**

Special Provisions for Waste Incineration Plants and Waste Co-Incineration Plants

Additionally, the IED comprises provisions on

- **Integrated Pollution Prevention and Control (IPPC)** and the
- **BAT Reference Document on Waste Incineration (BREF WI)**
apply for waste Incineration / co-incineration plants with capacities of
 - **> 3 tonnes per hour of non-hazardous waste**
 - **> 10 tonnes per day of hazardous waste**

IED Chapter IV & Annex VI: Scope of Waste

- Stationary and mobile waste incineration / co-incineration plants treating **solid and liquid waste**.
- **Exceptions:** Plants treating only
 - **vegetable waste**, e.g. from agriculture / forestry / food processing (exception: waste containing **halogenated organic compounds** or **heavy metals**),
 - **radioactive waste**,
 - **animal carcasses**,
 - waste resulting from the exploration for, and the exploitation of, **oil and gas** resources from **off-shore** installations and incinerated on board the installations,
 - **experimental plants** used for research/development/testing for **< 50 tonnes** of waste/year.

IED Chapter IV & Annex VI: Scope of Installations (1)

Waste Incineration Plants

- dedicated to the thermal treatment of waste,
- with or without recovery of the combustion heat.

Typical installation:

- **Municipal Solid Waste Incinerator (MSWI)**

Waste Co-incineration Plants

- **Main purpose:**
generation of energy or production of material products
- using waste as regular or additional fuel

3 types of plants:

- a) Cement kilns
- b) (Large) Combustion plants
- c) Co-incineration plants in other industrial sectors.

IED Chapter IV & Annex VI: Scope of Installations (2)

Waste incineration plants and waste co-incineration plants according to IED also include **“other thermal treatment processes”** such as

- **Pyrolysis,**
- **Gasification,**
- **Plasma Process,**

if the substances resulting from the treatment are subsequently incinerated.

IED Chapter IV & Annex VI: Permit Conditions

- List of all **waste types** which may be treated + their **quantities**,
- Total waste **capacity** of the plant,
- **Limit values** for **emissions into air and water**,
- Requirements for **wastewater discharges** (pH, temperature, flow),
- **Sampling and measurement** (procedures, measurements),
- **Maximum permissible period during which emissions may exceed the limit values** (e.g. due to technically unavoidable stoppages, disturbances, or failures of the purification devices or measurement devices),
- **Additional requirements when hazardous waste is incinerated**, e.g. lowest and maximum **calorific values** and their maximum contents of **polychlorinated biphenyls (PCBs)**, **pentachlorophenol (PCP)**, **chlorine**, **fluorine**, **sulphur**, **heavy metals** and other polluting substances.

IED ELVs for Air Emissions from WI: Continuous Monitoring, Daily Averages (DA)

1.1. Daily average emission limit values for the following polluting substances (mg/Nm³)

| | |
|--|-----|
| Total dust | 10 |
| Gaseous and vaporous organic substances, expressed as total organic carbon (TOC) | 10 |
| Hydrogen chloride (HCl) | 10 |
| Hydrogen fluoride (HF) | 1 |
| Sulphur dioxide (SO ₂) | 50 |
| Nitrogen monoxide (NO) and nitrogen dioxide (NO ₂), expressed as NO ₂ for existing waste incineration plants with a nominal capacity exceeding 6 tonnes per hour or new waste incineration plants | 200 |
| Nitrogen monoxide (NO) and nitrogen dioxide (NO ₂), expressed as NO ₂ for existing waste incineration plants with a nominal capacity of 6 tonnes per hour or less | 400 |

IED ELVs for Air Emissions from WI: Continuous Monitoring, Half-hourly Averages (HHA)

1.2. Half-hourly average emission limit values for the following polluting substances (mg/Nm³)

| | (100 %) A | (97 %) B |
|--|-----------|----------|
| Total dust | 30 | 10 |
| Gaseous and vaporous organic substances, expressed as total organic carbon (TOC) | 20 | 10 |
| Hydrogen chloride (HCl) | 60 | 10 |
| Hydrogen fluoride (HF) | 4 | 2 |
| Sulphur dioxide (SO ₂) | 200 | 50 |
| Nitrogen monoxide (NO) and nitrogen dioxide (NO ₂), expressed as NO ₂ for existing waste incineration plants with a nominal capacity exceeding 6 tonnes per hour or new waste incineration plants | 400 | 200 |

IED ELVs for Air Emissions from WI: Discontinuous Monitoring

| Parameter | Duration | ELV [mg/Nm ³] |
|---|---------------------|---------------------------|
| Hg * | 0.5 – 8 hours | 0.05 |
| Σ Cd + Tl * | 0.5 – 8 hours | 0.05 |
| Σ Sb + As + Pb + Cr + Co + Cu + Mn + Ni + V | 0.5 – 8 hours | 0.5 |
| PCDD/F | 6 – 8 hours | 0.000001 |
| CO | Daily average | 50 |
| CO | Half-hourly average | 100 |
| CO | 10 min average | 150 |

*) and their compounds

IED ELVs for Air Emissions from WI: Reference Conditions

- **Dry flue gas**
- **Pressure: 1 atm = 1,013 bar(a)**
- **Temperature: 0 °C**
- **O₂ concentration in the flue gas: 11 Vol%**
- Calculation of emitted pollutant loads:
Also the flue gas output in [m³] has to be re-calculated in order to comply with the reference conditions.
- If (also) **hazardous waste** is incinerated and the **actual O₂ content is <11 Vol%**, ELVs refer to actual O₂ concentration
→ **no „mathematical dilution“ is allowed.**

$$E_s = \frac{21 - O_s}{21 - O_M} \times E_M$$

E_s : Emission concentration, reference cond.

E_M : Emission concentration, measured

O_s : O₂ content, reference conditions

O_M : O₂ content, measured

IED ELVs for Discharges of Waste Water from the Cleaning of Waste Gas from WI

| Polluting substances | Emission limit values for unfiltered samples (mg/l except for dioxins and furans) | |
|---|--|----------|
| | (95 %) | (100 %) |
| 1. Total suspended solids as defined in Annex I of Directive 91/271/EEC | 30 | 45 |
| 2. Mercury and its compounds, expressed as mercury (Hg) | | 0,03 |
| 3. Cadmium and its compounds, expressed as cadmium (Cd) | | 0,05 |
| 4. Thallium and its compounds, expressed as thallium (Tl) | | 0,05 |
| 5. Arsenic and its compounds, expressed as arsenic (As) | | 0,15 |
| 6. Lead and its compounds, expressed as lead (Pb) | | 0,2 |
| 7. Chromium and its compounds, expressed as chromium (Cr) | | 0,5 |
| 8. Copper and its compounds, expressed as copper (Cu) | | 0,5 |
| 9. Nickel and its compounds, expressed as nickel (Ni) | | 0,5 |
| 10. Zinc and its compounds, expressed as zinc (Zn) | | 1,5 |
| 11. Dioxins and furans | | 0,3 ng/l |

Further Relevant Regulations of the IED (Examples)

- **Operating Conditions**
 - <3% TOC in solid residues,
 - Flue gas $\geq 850^{\circ}\text{C}$ (hazardous waste: 1100°C) for ≥ 2 seconds,
 - Heat recovery as far as practicable
 - Infectious clinical waste: straight into the furnace (no direct handling, no mixing with other waste categories),
 - Operation and control of the plant by a competent person etc.
- **Reception of Waste**
- **Reporting Obligations**
- **Residues**
 - amount and harmfulness shall be minimized,
 - shall be recycled, where appropriate;
 - no dispersal in the environment.
- **Provisions for Site Closure (definitive cessation of activity)**
 - including Baseline Report
- **Information of the Public**
- **Best Available Technique has to be applied → BREF Waste Incineration**

BREF Waste Incineration (1)

- **Defines the State of the Art in Waste Incineration.**
 - **BAT:**
Best Available Technique
 - **BREF:**
BAT Reference Document
 - Technique means more than Technology!
 - Developed in the so-called Sevilla Process of the European Commission.
 - Existing BREF WI from 2006
 - BREF WI Revision 2014-2018
 - Publication of revised BREF WI to be expected this year (2019)
 - **BAT-AELs:**
BAT Associated Emission Levels.
They correspond with BAT operation.
They are no ELVs...
 - **... but all over the EU, operating permits have to comply with them within 4 years after publication.**
- Information:
<http://eippcb.jrc.ec.europa.eu/reference/>

Annexes

8.7 Half-hourly and monthly average emission levels achieved by the waste incineration plants reporting continuously monitored emissions in the 2016 data collection: detailed graphs

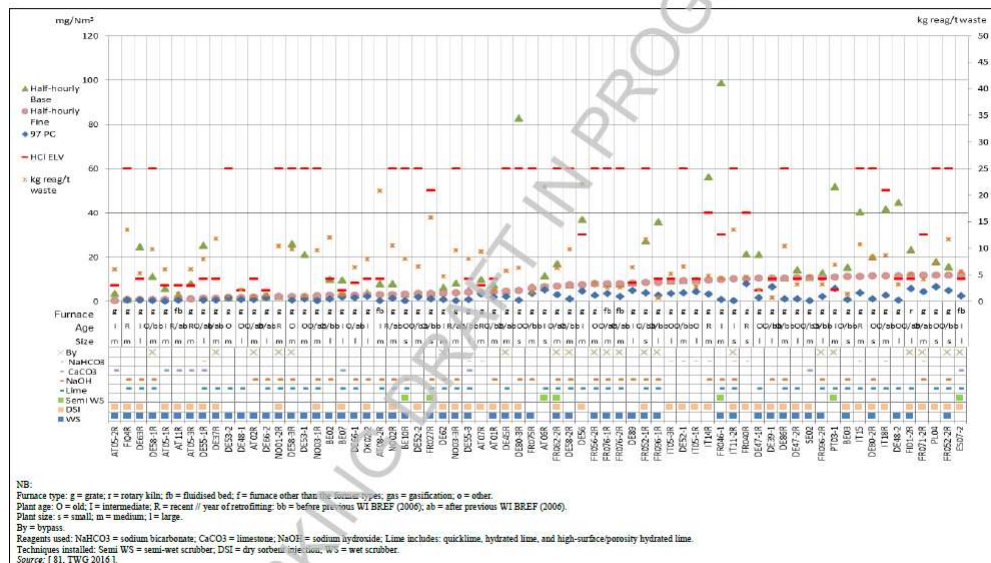


Figure 8.51: Half-hourly average emission levels for continuously monitored HCl emissions to air from reference lines incinerating predominantly MSW (1/3)

598

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BREF WI (Chapter 5): BAT Conclusions

- BAT 1 Environmental Management System
- BAT 2 – BAT 8 Monitoring
- BAT 9 – BAT 18 General Environmental and Combustion Performance
- BAT 19 – BAT 20 Energy Efficiency
- BAT 21 – BAT 24 Air Emissions - Diffuse Emissions
- BAT 25 – BAT 31 Air Emissions - Channelled Emissions
- BAT 32 – BAT 34 Emissions to Water
- BAT 35 – BAT 36 Material Efficiency
- BAT 37 Noise

BREF WI (Chapter 5) - Example Section of BAT 30 (Auszug)

Table 5.5: BAT-associated emission levels (BAT-AELs) for channelled emissions to air of TVOC, PCDD/F and dioxin-like PCBs from the incineration of waste

| Parameter | Unit | BAT-AEL | | Averaging period |
|--|----------------------------|-------------|----------------|--|
| | | New plant | Existing plant | |
| TVOC | mg/Nm ³ | < 3–10 | < 3–10 | Daily average |
| PCDD/F ⁽¹⁾ | ng I-TEQ/Nm ³ | < 0.01–0.04 | < 0.01–0.06 | Average over the sampling period |
| | | < 0.01–0.06 | < 0.01–0.08 | Long-term sampling period ⁽²⁾ |
| PCDD/F + dioxin-like PCBs ⁽¹⁾ | ng WHO-TEQ/Nm ³ | < 0.01–0.06 | < 0.01–0.08 | Average over the sampling period |
| | | < 0.01–0.08 | < 0.01–0.1 | Long-term sampling period ⁽²⁾ |

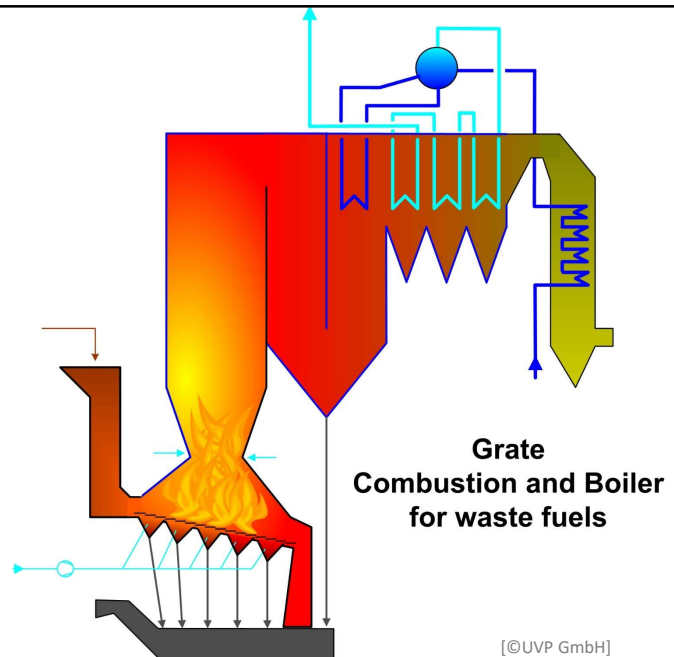
⁽¹⁾ Either the BAT-AEL for PCDD/F or the BAT-AEL for PCDD/F + dioxin-like PCBs applies.
⁽²⁾ The BAT-AEL does not apply if the emission levels are proven to be sufficiently stable.

WASTE INCINERATION TECHNOLOGY

Incineration Technology

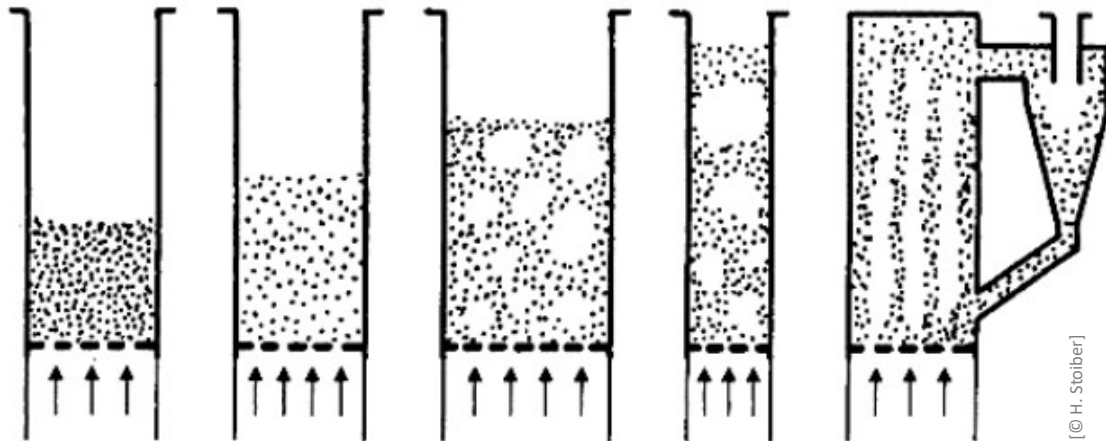
- **Grate Firing**
Standard Process for MSW Incineration
(Pre-treated) MSW, various waste fractions
- **Fluidized Bed Reactor**
Bubbling Fluidized Bed (BFB)
Circulating Fluidized Bed (CFB)
Pre-treated MSW, various pre-treated waste fractions
- **Rotary Kiln**
Hazardous Waste

Grate Firing



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Fluidized Bed

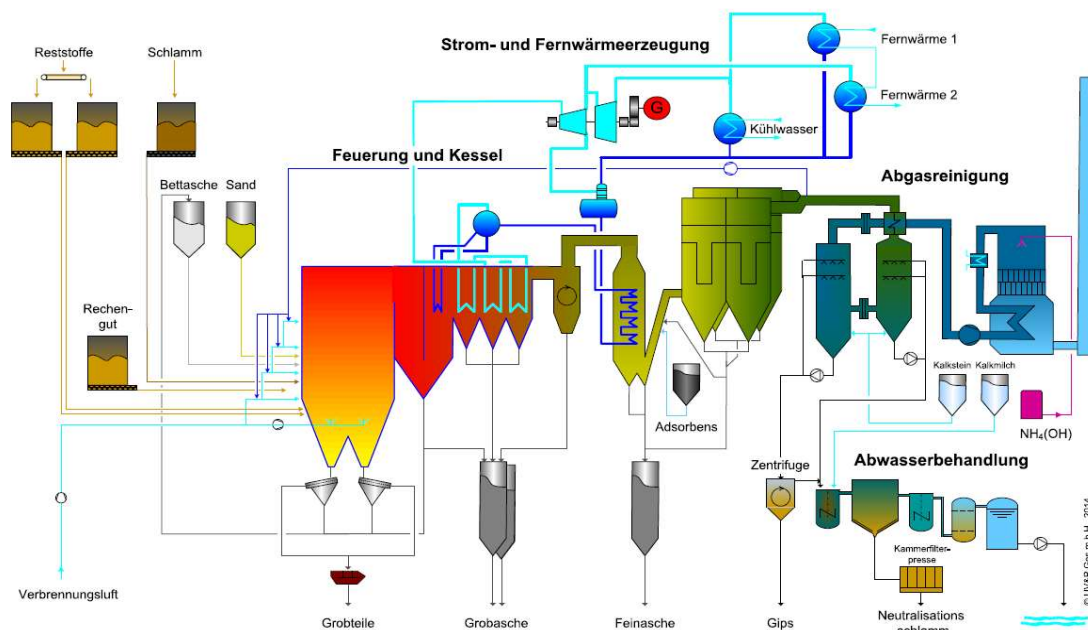


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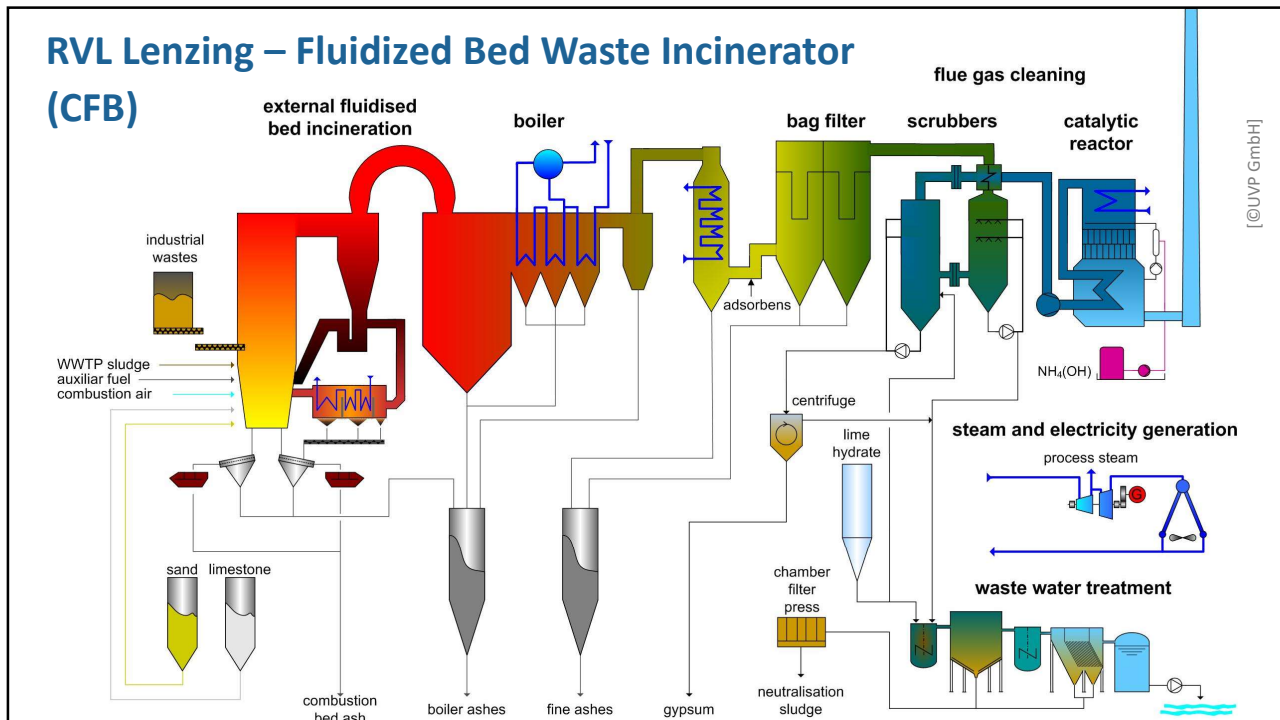
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RHKW Linz – Fluidized Bed Waste Incinerator (BFB)



236_7_3 Prinzipschema RHKW Linz_02-09-2014.vsd



Overview: Grate – Fluidized Bed – Rotary Kiln

Grate Firing

- Standard Process for MSWI
- LCV range ca. 8 – 12 MJ/kg
- 850° C
- **MSW (+ certain amounts of sewage sludge, shredded bulky waste ...)**

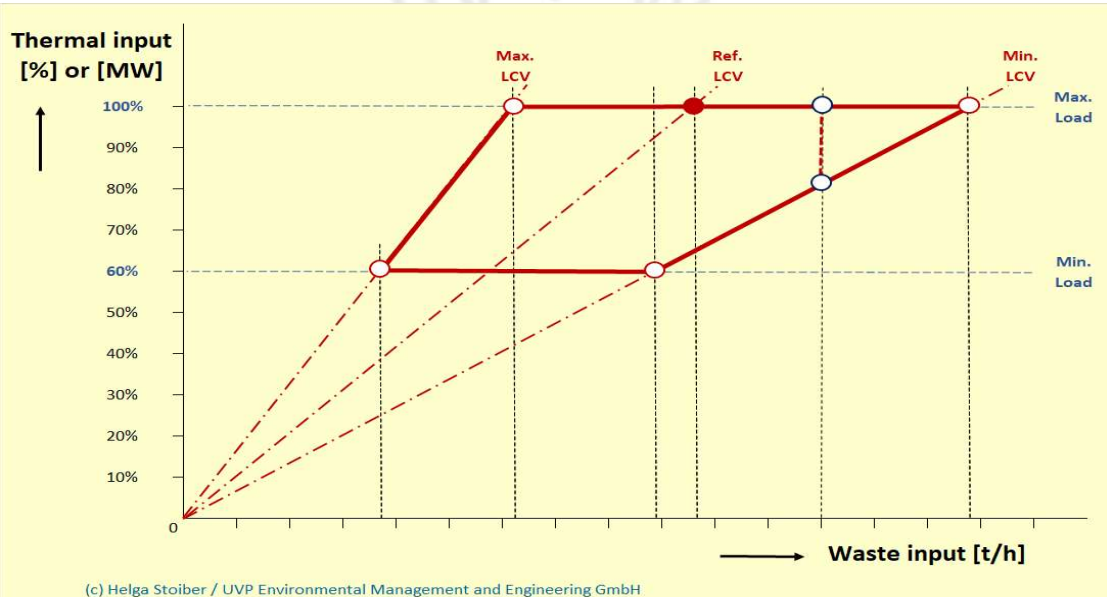
Rotary Kiln

- 1100 °C
- **Hazardous waste**

Fluidized Bed Incinerator

- 850° C
- Solid waste has to be mechanically pre-treated.
- LCV range ca. 3 – 35 MJ/kg →
- → High fuel flexibility
- **Pre-treated MSW, RDF, residues from mechanical or mechanical-biological waste treatment, plastic waste, sewage sludge, shredded bulky waste, rejects from paper recycling, ...**

Operating Diagram of a WI Plant



FLUE GAS CLEANING AFTER WASTE INCINERATION

Techniques to reduce Air Emissions (1)

- Cyclone
- Baghouse filter (Textile filter)
- Catalytic filter bags
- Electrostatic Precipitator (ESP)
- Direct desulphurisation
- Boiler sorbent injection
- Coarse Dust (no stand-alone de-dusting!)
- Dust, Adsorbents from dry injection
- PCDD/F, NO_x (when NH₃ is added)
- Dust
- SO_x (by addition of Mg or Ca based adsorbents directly into the fluidized bed)
- SO_x, HCl, HF (by injection of Mg or Ca based adsorbents into the post-combustion chamber)

Techniques to reduce Air Emissions (2)

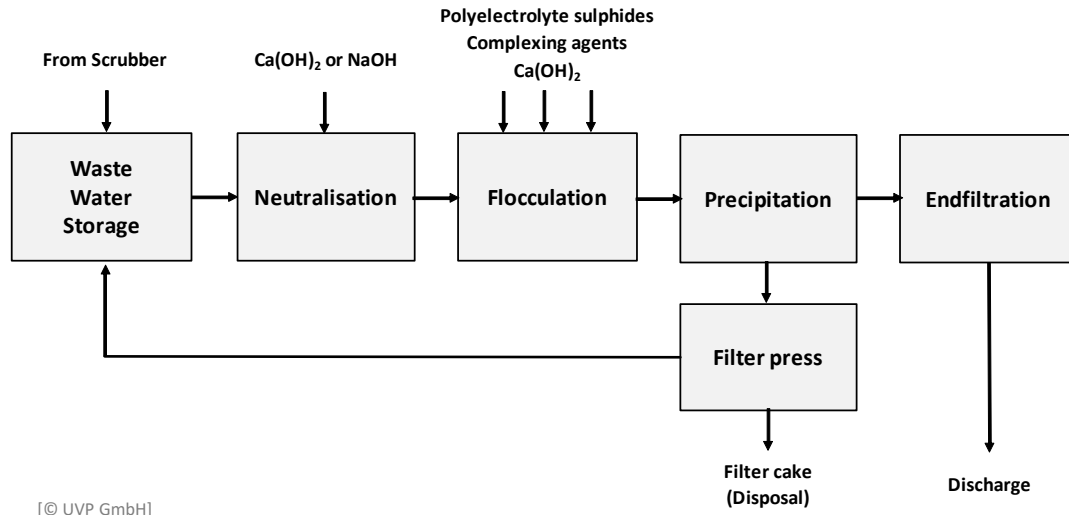
- Dry sorbent injection
 - Injection of a dry sorbent into the flue gas
SO_x, HCl, HF - Ca(OH)₂, NaHCO₃
PCDD/F, Hg(0) - Activated carbon
 - Hg(0) - Activated carbon, activated lignite...
- Fixed bed or Moving Bed Adsorption
- Flue gas recirculation
- Selective non-catalytic reduction (SNCR)
- Selective catalytic reduction (SCR)
 - NO_x – Reduction of NO_x formation by reducing the O₂ content in the furnace and by cooling
 - Reduction of NO_x by NH₃ injection into the flue gas at 800-1000 °C → N₂ formation
 - Reduction of NO_x by NH₃ injection into the flue gas at 200-400 °C in the presence of a catalyst → N₂ formation

Techniques to reduce Air Emissions (3)

- **Semi-wet absorber (Semi-wet absorber)**
- **Wet scrubber**
- **SO_x, HCl, HF** - Injection of an alkaline aqueous solution into the flue gas, product is dry
- **SO₂, HCl, HF, Hg(I, II)** - Water or aqueous solutions/suspensions of alkaline salts or lime are used as absorbent.

WASTE WATER TREATMENT AFTER WASTE INCINERATION

Waste Water Treatment - Example



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ENERGY RECOVERY

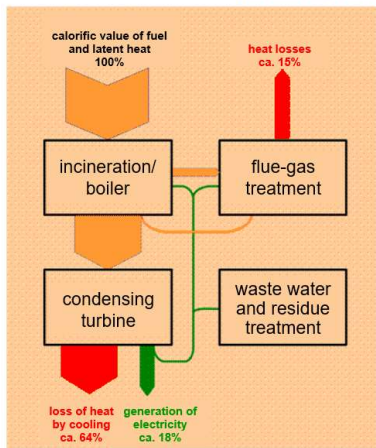
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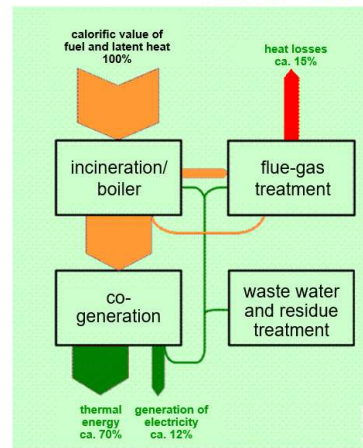
Site-specific Options for Energy Utilization

Condensing Turbine (electricity only)



Energy utilization approx. 20 %

Co-Generation (electricity + heat)



Energy utilization approx. 80 %

Site selection is crucial for energy efficiency!

Possible energy customers:

- **Process heat** (steam) for nearby industrial sites
- **District heating** for nearby municipalities
- **District cooling** for nearby municipalities
- Heat & electricity use in a nearby **seawater desalination** plant.

PYROLYSIS AND GASIFICATION OF WASTE

Process Characteristics (1)

| | COMBUSTION | GASIFICATION | PYROLYSIS |
|-------------------|------------------------------|---------------------------------|----------------------------------|
| Oxygen | $\lambda > 1$ | $\lambda < 1$ | $\lambda \sim 0$ |
| Medium | Air | Air, Steam | Steam, Inert Gas |
| Reaction Enthalpy | Exothermic $\Delta H > 0$ | Endothermic $\Delta H < 0$ | Endothermic $\Delta H < 0$ |
| Product | Flue Gas, Solid Residue | Synthesis Gas, Solid Residue | Gas, Tar, Coke, Solid Residue |

Process Characteristics (2)

| | COMBUSTION | GASIFICATION | PYROLYSIS |
|----------------|--|--|--|
| Products (Gas) | CO ₂ H ₂ O SO ₂ NO _x HCl, HF ... | CO ₂ , CO H ₂ O, H ₂ SO ₂ , H ₂ S NO _x , NH ₃ HCl, HF ... | CO ₂ , CO H ₂ O, H ₂ SO ₂ , H ₂ S, R-SH, R-S-R NO _x , NH ₃ , R-NH ₂ , ... HCl, HF ... Alkanes, Alkenes, Alkines Organic S-Compounds Organic N-Compounds Organic Cl-Compounds ... |

Process Characteristics (3)

| | COMBUSTION | GASIFICATION | PYROLYSIS |
|--------------------------|------------------------|-------------------------------|---|
| Products (Liquid) | - | Tar (small amount) | Tar (considerable amount) CxHy in any form including POPs |
| Products (Solid) | Inerts max. 3% TOC | Inerts Low TOC | Inerts High TOC (carbon loaded with gaseous and liquid CxHy products) |
| Reaction | Can be well controlled | Can be fairly well controlled | Mere cracking of organic matter, can merely be controlled by p, T, time |

Gasification

- Under certain circumstances, gasification of waste may make sense.
- Not many installations in operation.
- According to IED, syngas must be cleaned before incineration. Otherwise, the entire combustion plant becomes a co-incineration installation. (Cf. ECJ Decisions Lahti I, Lahti II)

Example:

Gasification plant in **Lahti, Finland**:
Gasification of Wood Waste, Incineration of the Syngas in an adjacent LCP plant →
→ Good energy efficiency due to water/steam parameters of the LCP plant.

Pyrolysis

- Pyrolysis of waste has been subject to R&D since about 50 years.
 - **Up to now, no process has been developed that is ecologically and economically feasible.**
 - **Pyrolysis DOES NOT produce a „marketable Diesel oil“ (never).**
 - **Pyrolysis is NOT state-of-the-art and is NOT a technology for thermal treatment of MSW.**
- Pyrolysis for thermal waste treatment **makes sense only in very few special cases**, e.g.
- Removal of plastic insulation from **cables** as pre-treatment in copper recycling.
 - Removal of plastic pieces from **WEEE** as pre-treatment in rare earth metals recycling.
 - **Feedstock recycling** in the context of a mineral oil refinery.

Plastic Pyrolysis for Feedstock Recycling in a Refinery: OMV ReOil Pilot Project

Plastic waste is pyrolysed. The pyrolysis products are fed into the refinery and processed there together with the normal mineral oil feed-stock.

They contribute to the production and output of the refinery.

Information about the project:

<https://www.omv.com/de/bl og/reoil-aus-kunststoff-wieder-oel-gewinnen>



Thank you for your attention!

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